

Beggs - Brill model

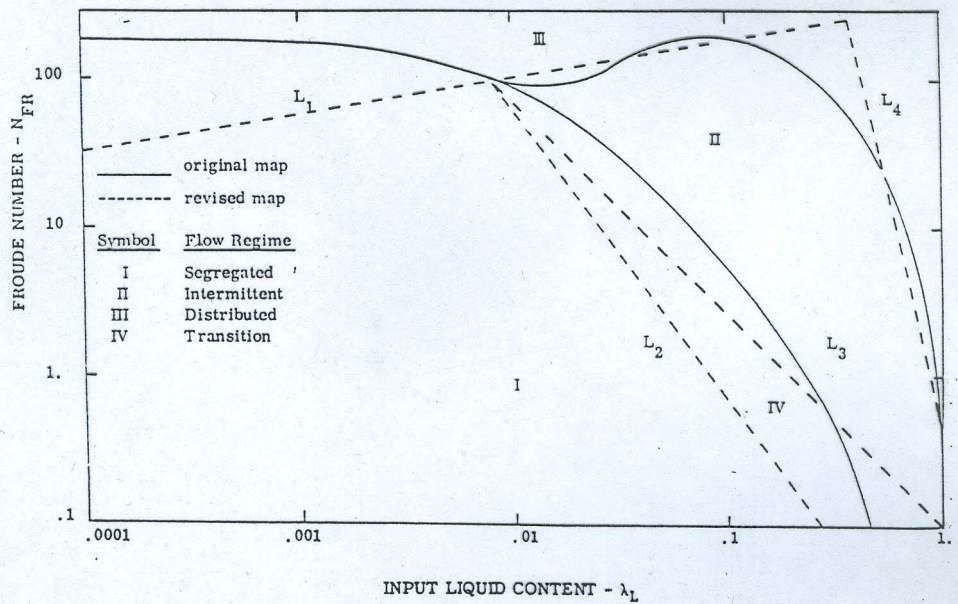
$$N_{FR} = \frac{V^2}{gD}$$

$$L_1 = 316\lambda_L^{0.302}$$

$$L_2 = 0.0009252\lambda_L^{-2.4684}$$

$$L_3 = 0.1\lambda_L^{-1.4516}$$

$$L_4 = 0.5\lambda_L^{-6.738}$$



HORIZONTAL FLOW PATTERN MAP

where:

$$\lambda_L = \frac{V_G}{V} \quad V = V_G + V_L$$

* Segregated flow pattern

$$\lambda_L < 0.01 \quad \text{and} \quad N_{FR} < L_1$$

or

$$\lambda_L > 0.01 \quad \text{and} \quad N_{FR} < L_2$$

* Distributed flow pattern

$$\lambda_L < 0.4 \quad \text{and} \quad N_{FR} > L_1$$

or

$$\lambda_L > 0.4 \quad \text{and} \quad N_{FR} > L_4$$

* Intermittent flow pattern

$$0.01 < \lambda_L < 0.4 \quad \text{and} \quad L_3 < N_{FR} < L_1$$

or

$$\lambda_L > 0.4 \quad \text{and} \quad L_3 < N_{FR} < L_4$$

* Transition

$$\lambda_L > 0.01 \quad \text{and} \quad L_2 < N_{FR} < L_3$$

Taitel - Dukler model for vertical pipes

a. Criterion for existence of bubble flow

$$\left[\frac{\rho_L^2 \cdot g \cdot D^2}{(\rho_L - \rho_G) \cdot \sigma} \right]^{1/4} \leq 4.36$$

b. Criterion for the transition from bubble to slug flow

$$V_L = 3.0V_G - 1.15 \left[\frac{g(\rho_L - \rho_G) \cdot \sigma}{\rho_L^2} \right]^{1/4}$$

c. Transition from bubble to dispersed bubble flow

$$V = 4.0 \left\{ \frac{D^{0.429} (\sigma/\rho_L)^{0.089}}{v_L^{0.072}} \cdot \left[\frac{g(\rho_L - \rho_G)}{\rho_L} \right]^{0.446} \right\}$$

d. Transition from dispersed bubble to slug flow

$$V_L = \frac{0.48}{0.52} \cdot V_G^{-0.48} \cdot 1.53 \left[\frac{g(\rho_L - \rho_G) \cdot \sigma}{\rho_L^2} \right]^{1/4}$$

e. Transition from slug to churn flow

$$\frac{l_e}{D} = 40.6 \left(\frac{V}{\sqrt{g}} + 0.22 \right)$$

f. Transition to Annular flow

$$\frac{V_G \cdot \rho_G^{1/2}}{[\sigma g(\rho_L - \rho_G)]^{1/4}} = 3.1$$

Taitel - Dukler model for horizontal and inclined pipes

$$\tilde{h}_L = \frac{h_L}{D}$$

$$\tilde{A}_L = \frac{A_L}{D^2} = 0.25 \left[\pi - \cos^{-1}(2\tilde{h}_L - 1) + (2\tilde{h}_L - 1) \sqrt{1 - (2\tilde{h}_L - 1)^2} \right]$$

$$\tilde{A}_G = \frac{A_G}{D^2} = 0.25 \left[\cos^{-1}(2\tilde{h}_L - 1) - (2\tilde{h}_L - 1) \sqrt{1 - (2\tilde{h}_L - 1)^2} \right]$$

$$\tilde{P}_i = \frac{P_i}{D} = \sqrt{1 - (2\tilde{h}_L - 1)^2}$$

$$\tilde{u}_G = \frac{u_G}{V_G} = \frac{\tilde{A}}{\tilde{A}_G} \quad \tilde{u}_L = \frac{u_L}{V_L} = \frac{\tilde{A}}{\tilde{A}_L}$$

$$\tilde{A} = \frac{A}{D^2}$$

$$\tilde{P}_L = \frac{P_L}{D} = \pi - \cos^{-1}(2\tilde{h}_L - 1) \quad \tilde{P}_G = \frac{P_G}{D} = \cos^{-1}(2\tilde{h}_L - 1)$$

$$\tilde{D}_L = \frac{4A_L}{P_L \cdot D} = \frac{4\tilde{A}_L}{\tilde{P}_L} \quad \tilde{D}_G = \frac{4A_G}{D(P_G + P_i)} = \frac{4\tilde{A}_G}{\tilde{P}_G + \tilde{P}_i}$$

$$\tau_{OG} \cdot \frac{P_G}{A_G} - \tau_{OL} \cdot \frac{P_L}{A_L} + \tau_i P_i \left(\frac{1}{A_L} + \frac{1}{A_G} \right) - (\rho_L - \rho_G) g \sin \alpha = 0$$

$$\tau_{OL} = \frac{f_L \rho_L u_L^2}{2} \quad \tau_{OG} = \frac{f_G \rho_G u_G^2}{2}$$

$$\tau_i = \frac{f_i \rho_G (u_G - u_L)^2}{2}$$

$$f_L = C_L \left(\frac{D_L u_L \rho_L}{\mu_L} \right)^{-n} \quad f_G = C_G \left(\frac{D_G u_G \rho_G}{\mu_G} \right)^{-m}$$

$$x^2 (\bar{u}_L \bar{D}_L)^{-n} \cdot \bar{u}_L^2 \frac{\bar{P}_L}{\bar{A}_L} - (\bar{u}_G \bar{D}_G)^{-m} \cdot \bar{u}_G^2 \left(\frac{\bar{P}_G}{\bar{A}_G} + \frac{\bar{P}_L}{\bar{A}_L} + \frac{\bar{P}_i}{\bar{A}_G} \right) - 4Y = 0$$

$$x^2 = \frac{(dP_F/dz)_L}{(dP_F/dz)_G} \quad Y = \frac{-(\rho_L - \rho_G) g \sin \alpha}{(dP_F/dz)_G}$$

$$k^2 = F^2 \cdot Re_L = \frac{\rho_G \cdot V_G^2}{(\rho_L - \rho_G) D g \cos \alpha} \cdot \frac{DV_L}{v_L}$$

$$F^2 \cdot \frac{1}{C_2^2} \cdot \frac{\bar{u}_G \cdot d\bar{A}_L / d\bar{h}_L}{\bar{A}_G} \geq 1$$

$$k > \frac{20}{\bar{u}_G \sqrt{\bar{u}_L}}$$

$$F = \sqrt{\frac{\rho_G}{\rho_L - \rho_G} \cdot \frac{u_G}{\sqrt{D g \cos \alpha}}}$$

$$T^2 < \frac{8\bar{A}_G}{\bar{P}_i \bar{u}_L^2 (\bar{u}_L \bar{D}_L)^{-n}}$$

$$C_2 = 1 - \bar{h}_L$$

$$T = \left[\frac{(dP_F/dz)_L}{(\rho_L - \rho_G) g \cos \alpha} \right]^{1/2}$$

Wallis model

$$u_G = C_o V + u_s \quad \text{where } C_o = 1.2 \text{ for slug flow}$$

$$V_i = \frac{[D^3 g (\rho_L - \rho_G) \rho_L]^{1/2}}{\mu_L}$$

$$E_o = \frac{g D^2 (\rho_L - \rho_G)}{\sigma}$$

$$\frac{u_s}{\sqrt{gD}} = 0.345 [1 - \exp(0.029 V_i)] \cdot \left(1 - \exp \frac{3.37 - E_o}{m} \right)$$

$$m = 10 \quad \text{for } V_i > 250$$

$$m = 69 \cdot V_i^{-0.35} \quad \text{for } 18 < V_i < 250$$

$$m = 25 \quad \text{for } V_i < 18$$

$$u_s = 0.345 \sqrt{gD}$$

$$e_G = \frac{V_G}{u_G}$$

Mukherjee - Brill model

$$H_L = \exp[(C_1 + C_2 \sin \alpha + C_3 \sin^2 \alpha + C_4 N_L^2)] \cdot \frac{N_{gV}^{C_5}}{N_{LV}^{C_6}}$$

$$N_L = \mu_L \cdot \left(\frac{g}{\rho_L \cdot \sigma^3} \right)^{0.25}$$

$$N_{gV} = V_G \cdot \left(\frac{\rho_L}{g \cdot \sigma} \right)^{0.25}$$

$$N_{LV} = V_L \cdot \left(\frac{\rho_L}{g \cdot \sigma} \right)^{0.25}$$

$C_1, C_2, C_3, C_4, C_5, C_6$: constants

Taitel - Dukler model

$$\epsilon_G = \frac{1}{\pi} \left[\cos^{-1}(2\tilde{h}_L - 1) - (2\tilde{h}_L - 1) \cdot \sqrt{1 - (2\tilde{h}_L - 1)^2} \right]$$

$$H_L = 1 - \epsilon_G$$