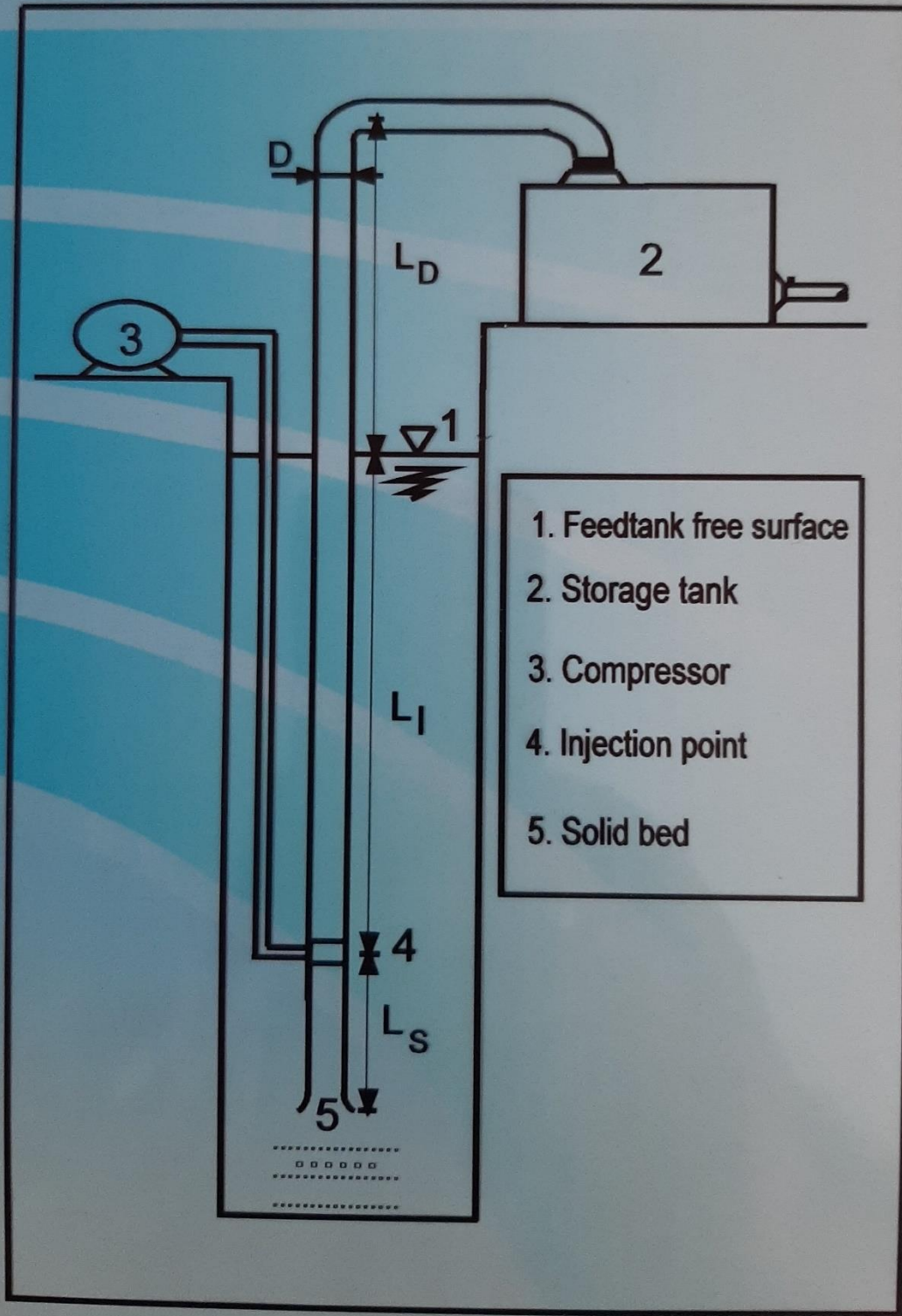
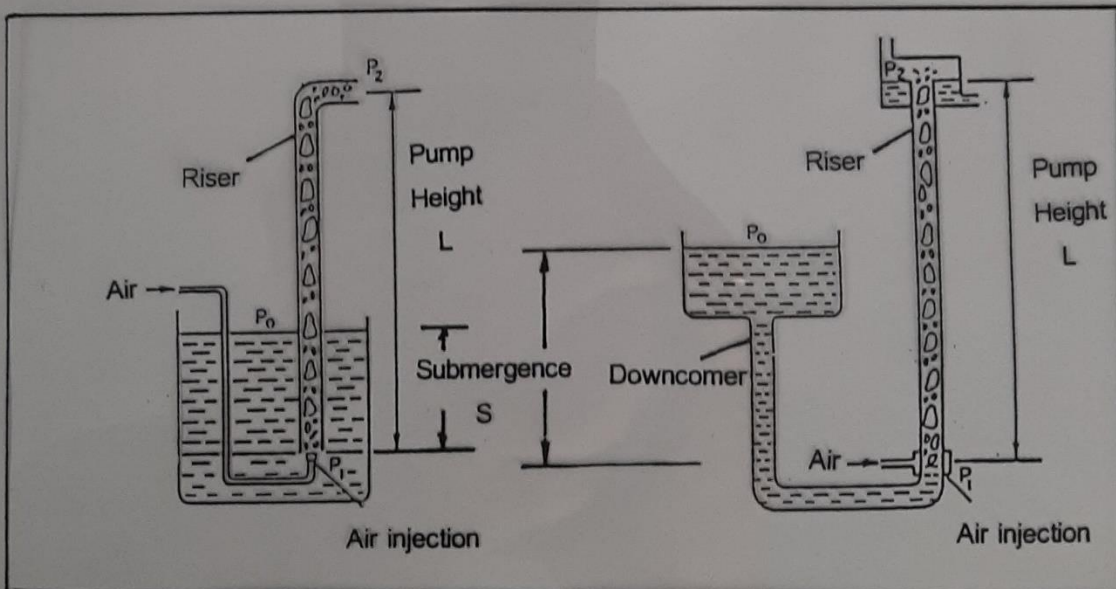
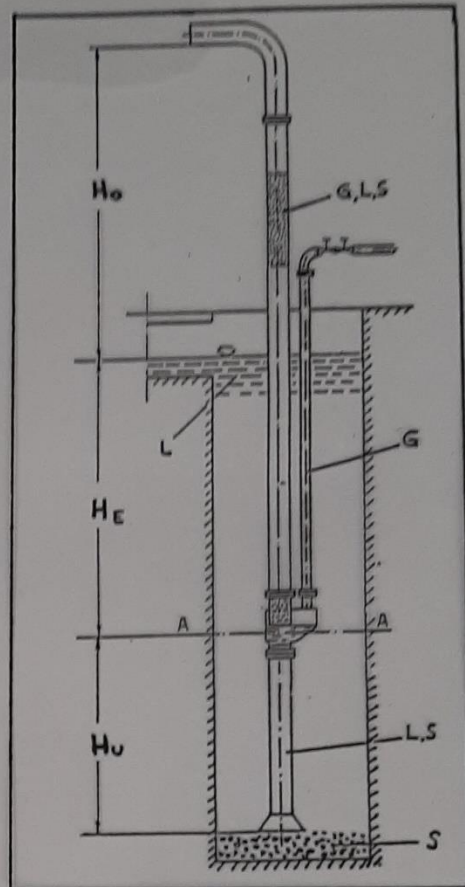
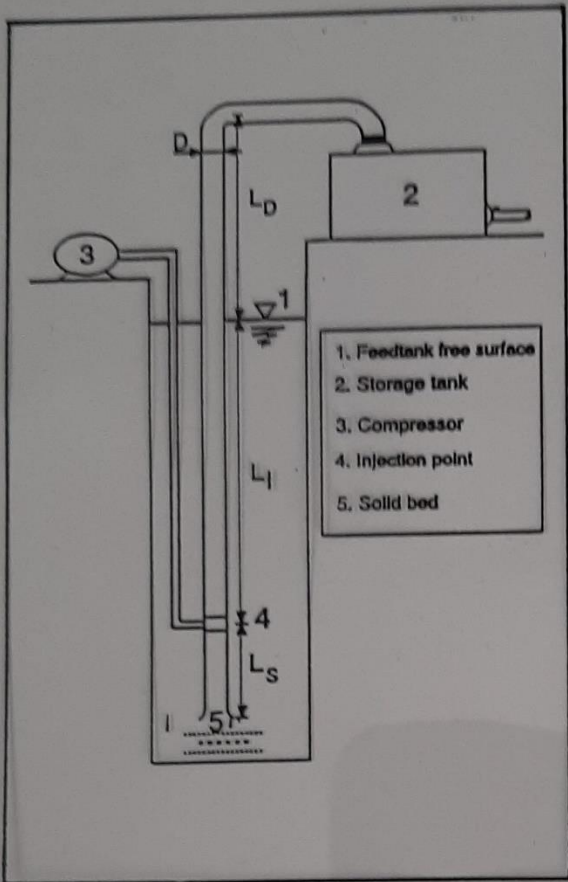


# Airlift pump installation



# AIR - LIFT PUMP



Εγκαταστάσεις Air-Lift Pump

# ΜΟΝΤΕΛΟ ΣΧΕΔΙΑΣΜΟΥ AIR-LIFT PUMP

## Ισορροπία πιέσεων

$$p_o + \rho_3 g(L_s + L_l) = p_n + \Delta p_{Tot}$$

## Απώλειες πίεσης στο πρώτο τμήμα

$$\Delta p_s = \int_0^{L_s} \frac{dp}{dx} dx = \Delta p_{\Delta x} L_s$$

## Απώλειες πίεσης στο δεύτερο και τρίτο τμήμα

$$\Delta p_{l,D} = \sum_i^K \left( \frac{\Delta p}{\Delta x} \right)_K \Delta x, \quad K = \frac{L_l + L_D}{\Delta x}$$

## Βαθμός απόδοσης

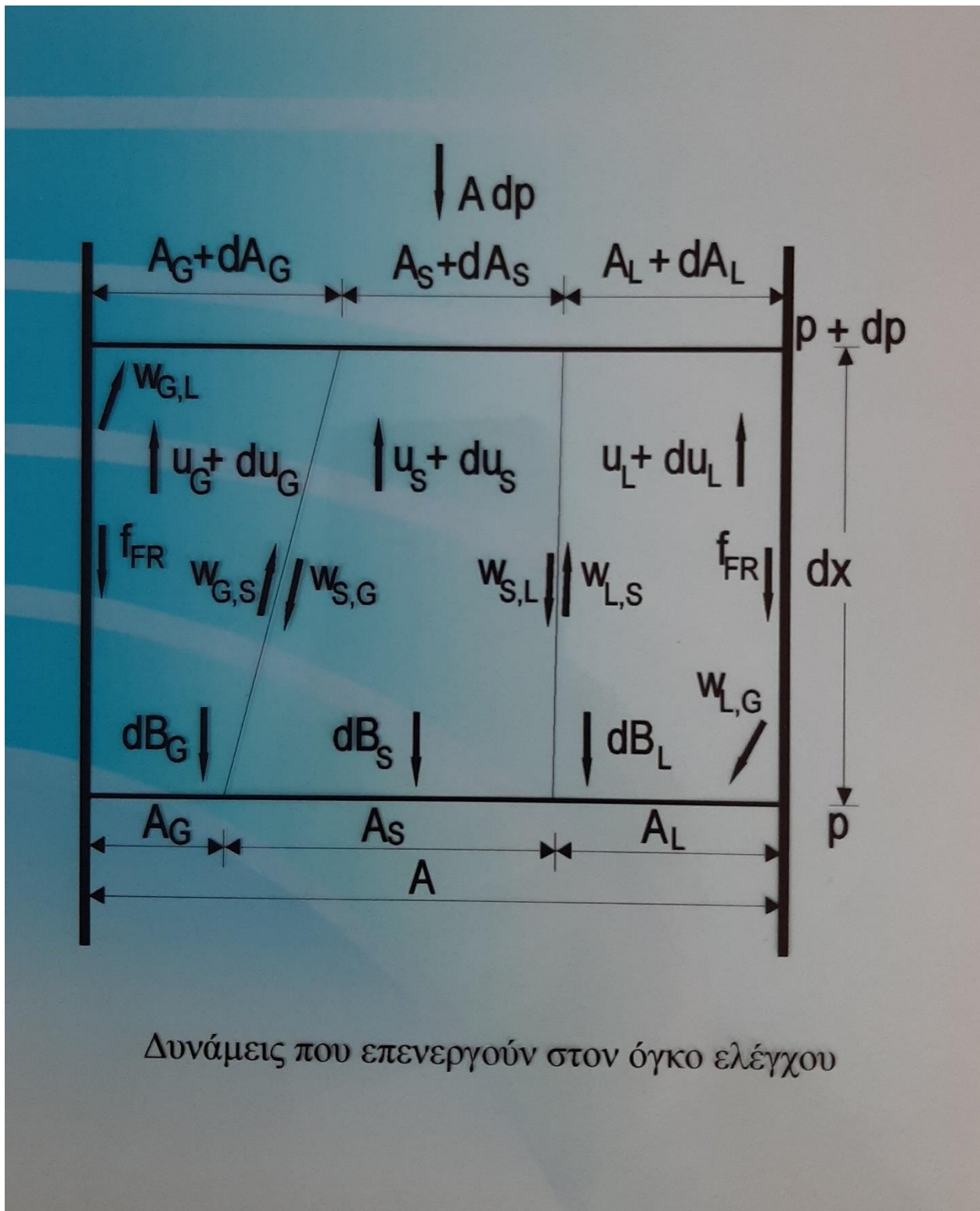
$$\eta = \frac{N_G}{N_C}$$

## Καταναλισκόμενη ισχύς

$$N_C = \int_{p_o}^{p_1} \frac{M_2}{\rho_2} dp = M_2 R T \ln \left( \frac{p_1}{p_o} \right)$$

## Ωφέλιμη ισχύς

$$N_G = C M_1 g \left( (L_s + L_l) \left( 1 - \frac{\rho_1}{\rho_3} \right) + L_D \right) + (1 - C) g L_D M_3$$



# ΦΥΣΙΚΟΜΑΘΗΜΑΤΙΚΟ ΜΟΝΤΕΛΟ

Εξισώσεις διατήρησης Χωριστής Τριφασικής Ροής

## Εξίσωση συνέχειας

$$M_t = \sum_{i=1}^3 M_i = \sum_{i=1}^3 \rho_i u_i A_i = \sum_{i=1}^3 \rho_i u_i a_i A = \text{const.} \quad \mu\epsilon \quad \sum_{i=1}^3 a_i = 1$$

## Εξίσωση ορμής

$$\sum F = \sum_{i=1}^3 \left( \underbrace{-\rho_i a_i A dx g}_{\text{Gravitational forces}} - \underbrace{\rho_i a_i A dx \frac{du_i}{dt}}_{\text{Acceleration forces}} - \underbrace{a_i A dp}_{\text{Pressure forces}} - \underbrace{a_i A dp_{FR,i}}_{\text{Friction forces}} + \underbrace{\sum_{j=1}^3 \delta_{i,j} w_{i,j}}_{\text{Interaction forces}} \right) = 0$$

$$-\frac{dp}{dx} = \sum_{i=1}^3 \left( \rho_i a_i g + \rho_i a_i u_i \frac{du_i}{dx} + \left( \frac{dp}{dx} \right)_{FR,i} \right)$$

## Απόλυτες και Σχετικές Ταχύτητες

$$u_i = u_3 + (-1)^i u_{i,r} \quad u_{i,r} = \left( \frac{4 d_i a_3 g}{3 C_{D,i}} \left| 1 - \frac{\rho_i}{\rho_3} \right| \right)^{\frac{1}{2}}$$

## Συντελεστής αντίστασης

$$C_{D,i} = \sum_{j=1}^2 B_{i,j} Re_i^{b_{i,j}} \quad | \quad i = 1, 2$$

## Αριθμός Reynolds

$$Re_i = \frac{\rho_3 |u_i - u_3| d_i}{\mu_3}$$

## Συντελεστής συμπιεστότητας

$$\frac{p}{Z\rho_2} = RT = \text{const.} \quad Z(p) = 1 - 5.8198 \cdot 10^{-4} \left( \frac{p_l}{p_n} \right) + 2.809 \cdot 10^{-6} \left( \frac{p_l}{p_n} \right)^2$$

## ΜΟΝΤΕΛΟ ΨΕΥΔΟ-ΥΓΡΟΥ

$$\rho_{PS} = \left( \frac{a_1}{a_{PS}} \right) \rho_1 + \left( \frac{a_3}{a_{PS}} \right) \rho_3 = \alpha_1^* \rho_1 + \alpha_3^* \rho_3 \quad \mu\epsilon \quad a_{PS} = a_1 + a_3$$

$$\mu_{PS} = (1 - c_m) \nu_3 \rho_{PS} \quad \acute{o}\pi\omega\upsilon \quad c_m = \frac{\rho_1}{\rho_{PS}} \left( \frac{a_1}{a_{PS}} \right)$$

$$M_{PS} = M_1 + M_2 = u_{PS} \rho_{PS} a_{PS} A$$

$$\left( \frac{dp}{dx} \right)_{FR} = \Phi_{PSO}^2 \left[ \left( \frac{dp}{dx} \right)_{FR} \right]_{PSO}$$

$$\Phi_{PSO}^2 = E + \frac{3.24FH}{Fr^{0.045} + We^{0.035}}$$

$$E = (1-x)^2 + x^2 \frac{\rho_{PS} f_{2O}}{\rho_2 f_{PSO}}$$

$$F = x^{0.78} (1-x)^{0.24}$$

$$H = \left( \frac{\rho_{PS}}{\rho_2} \right)^{0.91} \left( \frac{\mu_2}{\mu_{PS}} \right)^{0.19} \left( 1 - \frac{\mu_2}{\mu_{PS}} \right)^{0.7}$$

$$Fr = \frac{m^2}{gD\rho_{PST}^2}$$

$$We = \frac{m^2 D}{\sigma \rho_{PST}}$$

$$\rho_{PST} = \left( \frac{x}{\rho_2} + \frac{1-x}{\rho_{PS}} \right)^{-1}$$

ΠΙΝΑΚΑΣ 1 Σταθερές για τον υπολογισμό του συντελεστή αντίστασης σφαιρικών σωματιδίων ή φυσαλίδων

$Re_i$	$B_{11}$	$b_{11}$	$B_{12}$	$b_{12}$	$B_{21}$	$b_{21}$	$B_{22}$	$b_{22}$
$< 0.2$	24	-1	0	0	24	-1	0	0
$0.2 - 989$	26	0.8	0.4	0	3.6	-0.313	24	-1
$989 - 10^4$					0.44	0	0	0
$10^4 - 2 \times 10^5$	0.4	0	0	0				
$> 2 \times 10^5$	-	-	-	-	0.1	0	0	0

ΠΙΝΑΚΑΣ 2 Σταθερές για υπολογισμό του συντελεστή αντίστασης  
σωματιδίων διαφόρων σχημάτων ή σφαιρικών φυσαλίδων

<i>Constants</i>			<i>Reynolds range</i>	<i>Characteristic dimension</i>	<i>Shape of particle</i>	<i>Reference</i>
<i>B<sub>1</sub></i>	<i>B<sub>2</sub></i>	<i>B<sub>3</sub></i>				
24	0	0	$Re_1 < 0.1$	diameter	sphere	Stokes
24	4	0.4	$Re_1 < 10^4$	diameter	sphere	Molerus
21.5	6.5	0.23	$0.5 < Re_1 < 10^3$	diameter	sphere	Muschelk
24	6	0.35	$0.5 < Re_1 < 800$	1.5 x a a=larg dimen.	Polyhed.	Muschelk
23	6	0.5	$0.5 < Re_1 < 600$	1.08 x dz dz=base diam.	cylinder l/dz = 1	Muschelk
27	4.5	0.65	$0.5 < Re_1 < 400$	1.24 x a a= edge	cube	Muschelk



## ΑΡΙΘΜΗΤΙΚΗ ΛΥΣΗ

$$\frac{dp}{dx} = \sum_{i=1}^3 \left( \rho_i a_i g + \rho_i a_i u_i \frac{du_i}{dx} + \left( \frac{dp}{dx} \right)_{FR,i} \right)$$

$$u_i \rho_i \frac{da_i}{dx} + u_i a_i \frac{d\rho_i}{dx} + \rho_i a_i \frac{du_i}{dx} = 0$$

$$\mu\epsilon \quad \frac{d\rho_1}{dx} = \frac{d\rho_3}{dx} = 0 \quad \text{και} \quad \sum_{i=1}^3 \frac{da_i}{dx} = 0$$

$$\frac{du_i}{dx} = \frac{du_3}{dx} + (-1)^i \frac{du_{i,r}}{dx} \quad \frac{du_{1,r}}{dx} = \left( \frac{4 d_1 g}{3 C_{D,1}} \left( \frac{\rho_1 - 1}{\rho_3} \right) \right)^{\frac{1}{2}} \frac{1}{2a_3^{\frac{1}{2}}} \frac{da_3}{dx}$$

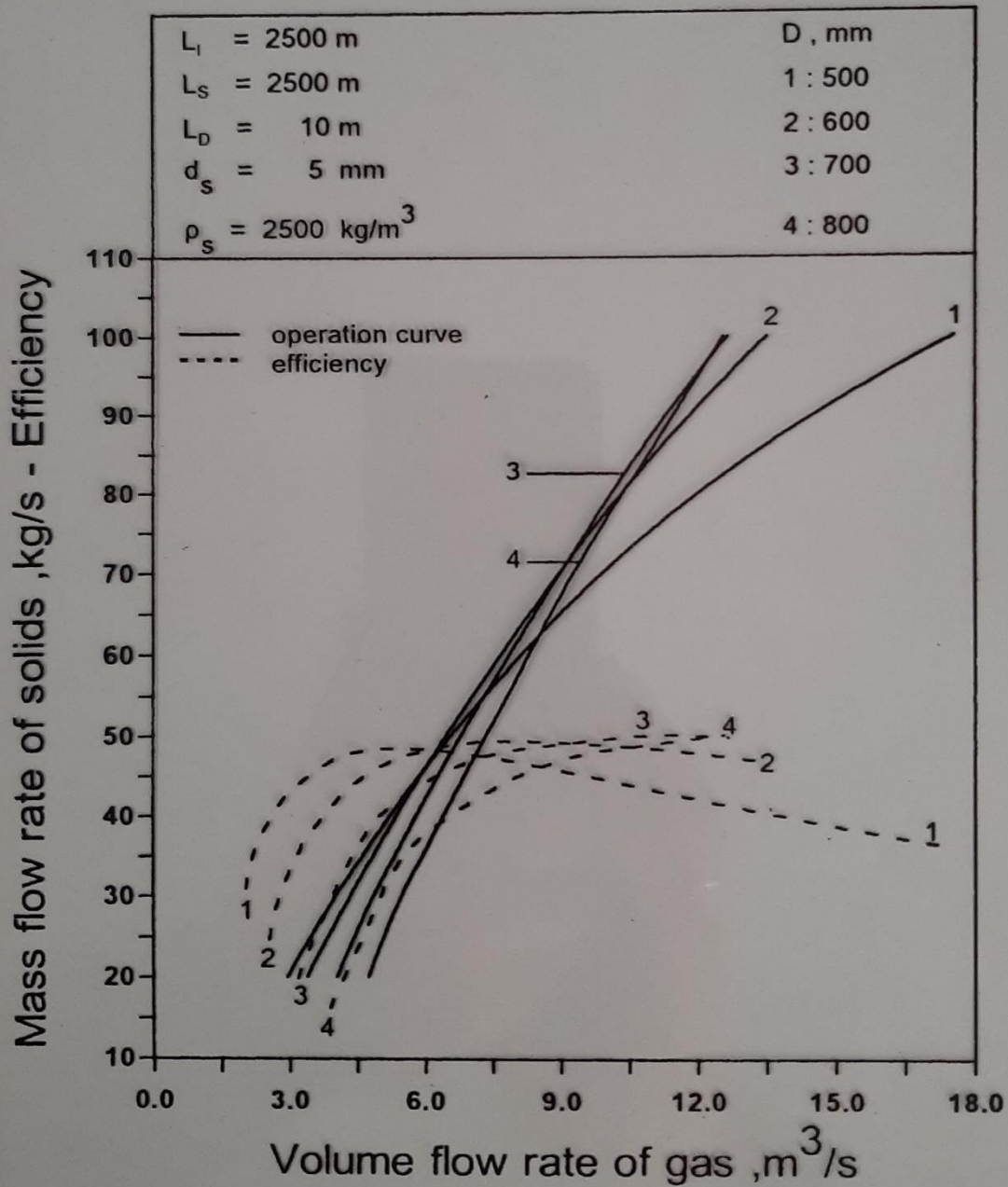
$$u_{2,r} = \left( \frac{4 d_{2,0} a_3 g}{3 C_{D,2}} \left( \frac{p_0}{Z_0} \right)^{\frac{1}{3}} \right)^{\frac{1}{2}} \left( 1 - \frac{Z_0 \rho_{2,0} p}{p_0 \rho_3 Z} \right)^{\frac{1}{2}} \left( \frac{Z}{p} \right)^{\frac{1}{6}}$$

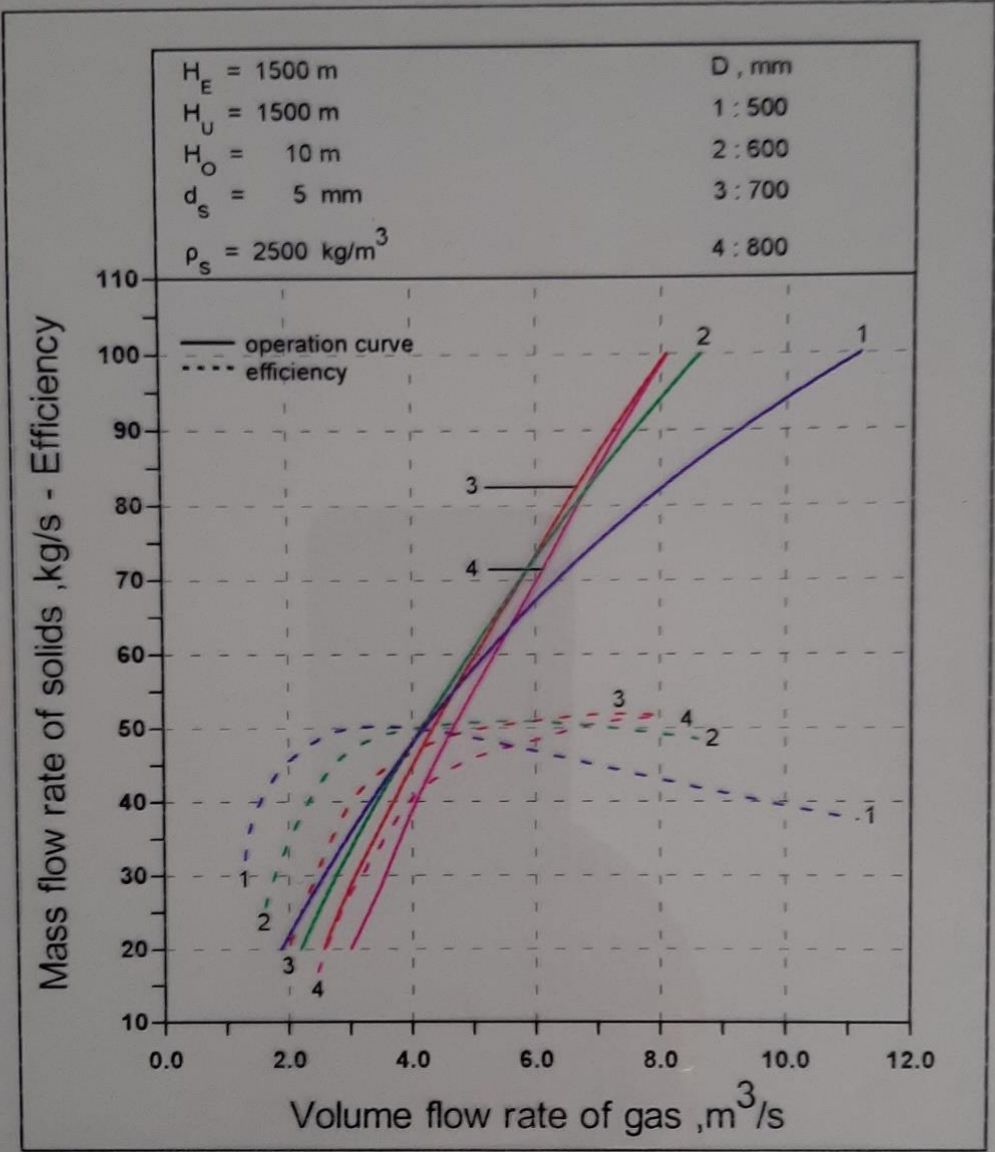
$$\frac{du_{2,r}}{dx} = C_1 \left( C_2 \left( Z^{-1} \frac{dZ}{dp} - p^{-1} \right) \right) \frac{dp}{dx} + \left( \frac{\rho_3 - \rho_2}{4\rho_3 a_3^2} \right)^{\frac{1}{2}} \frac{da_3}{dx}$$

$$C_1 = \left( \frac{4 d_{2,0} g a_3}{3 C_{D,2}} \right)^{\frac{1}{2}} \left( \frac{p_0}{p} \frac{Z}{Z_0} \right)^{\frac{1}{6}} \quad \text{και} \quad C_2 = \frac{1}{6} \frac{\rho_3 + 2\rho_2}{(2\rho_3 - \rho_2)^{\frac{1}{2}}}$$

$$\frac{dZ}{dx} = \left( \frac{dp}{dx} - \frac{p}{\rho_2} \frac{d\rho_2}{dx} \right) \frac{Z}{p}$$

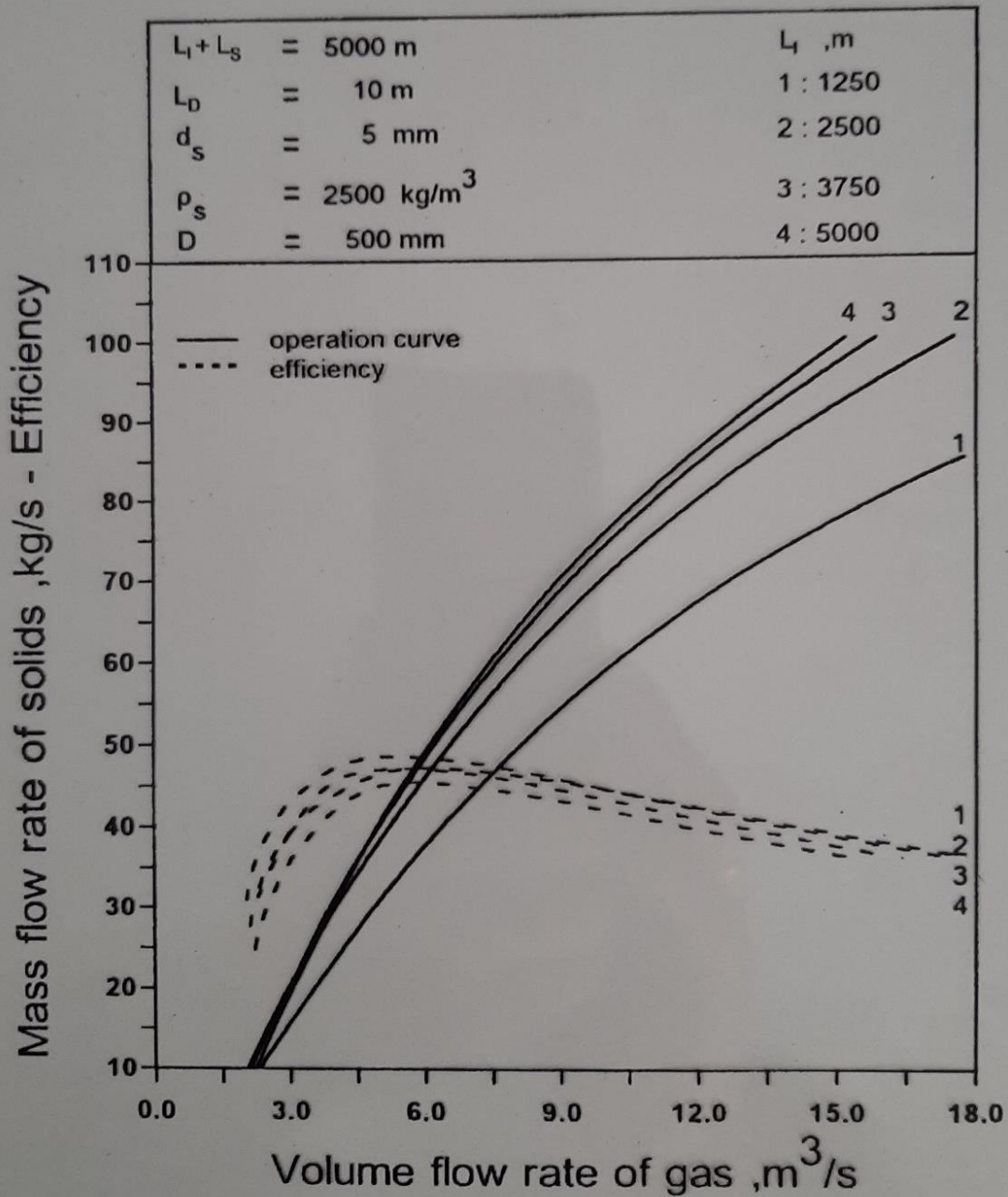
# Pipe diameter influence on the airlift pump efficiency

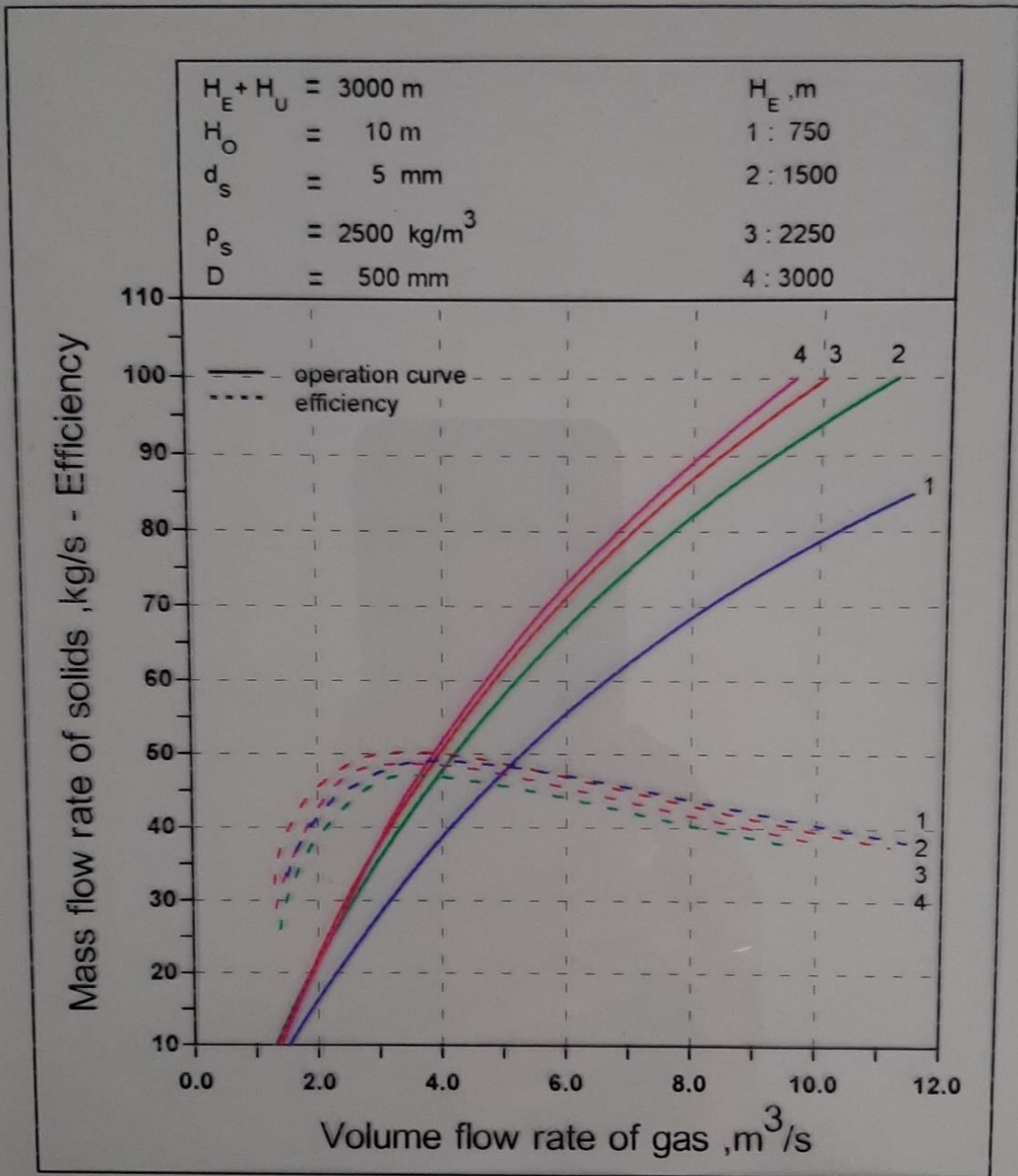




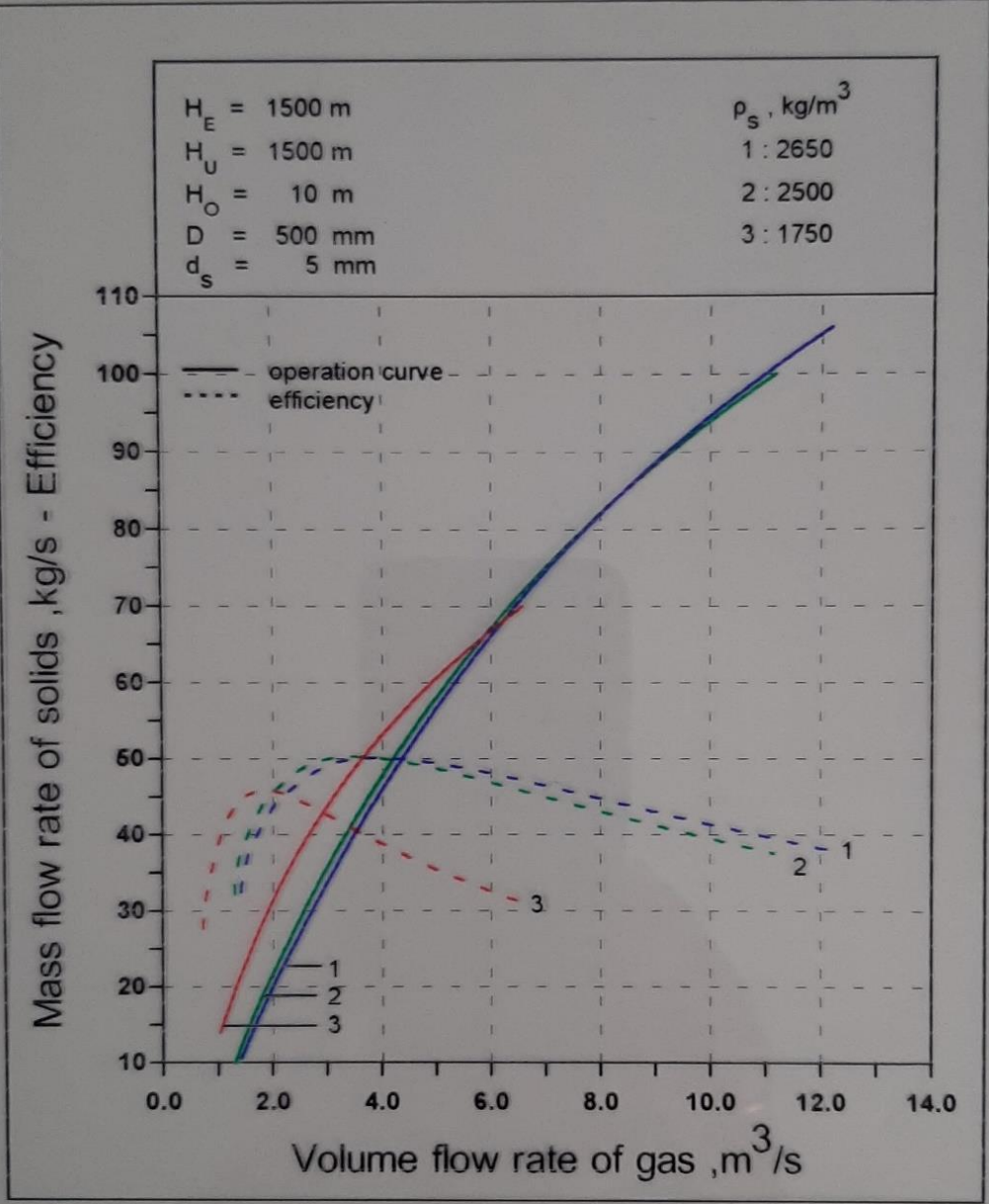
Influence of pipe diameter on Air - Lift pump operation

# Injection depth influence on the airlift pump efficiency

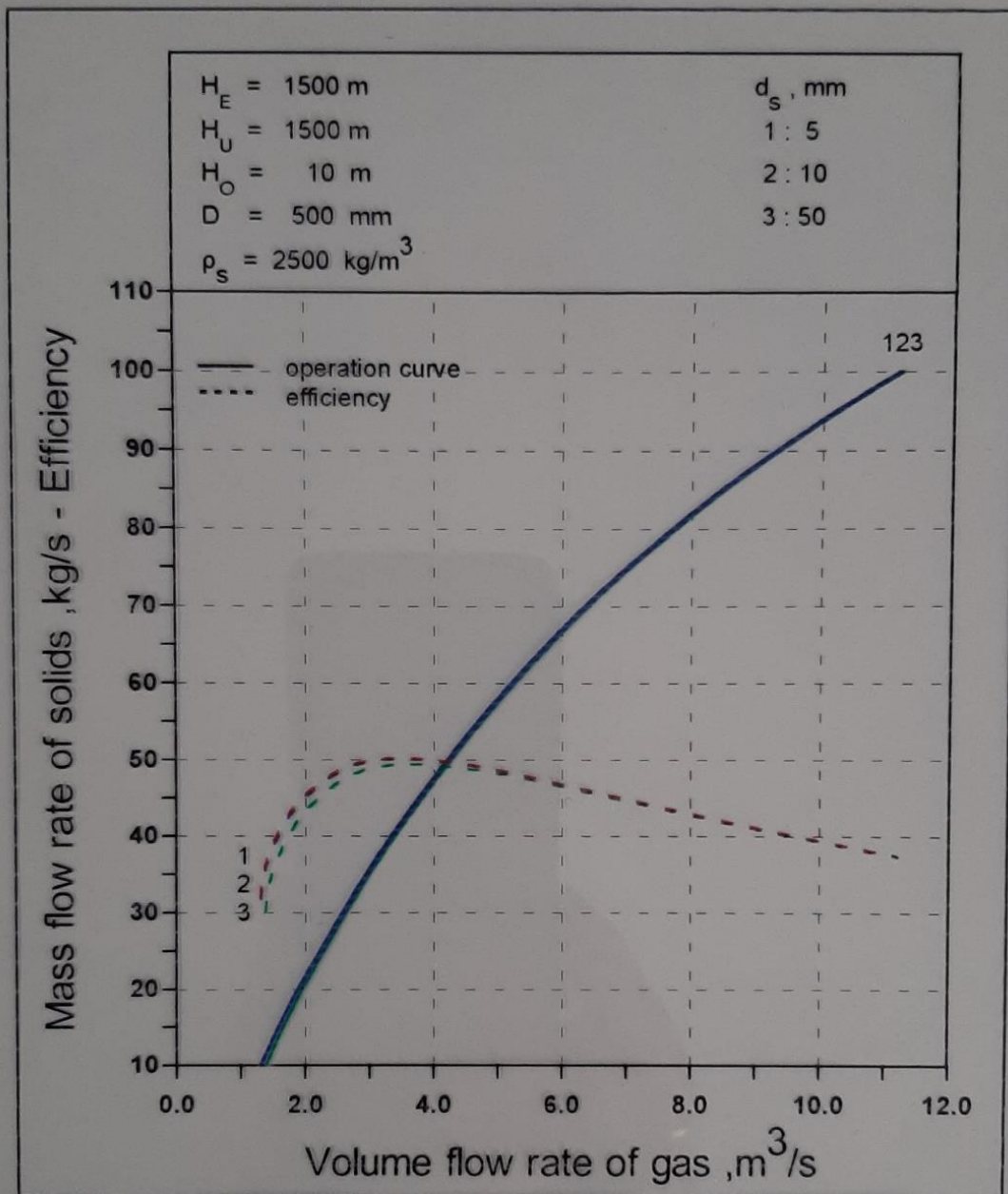




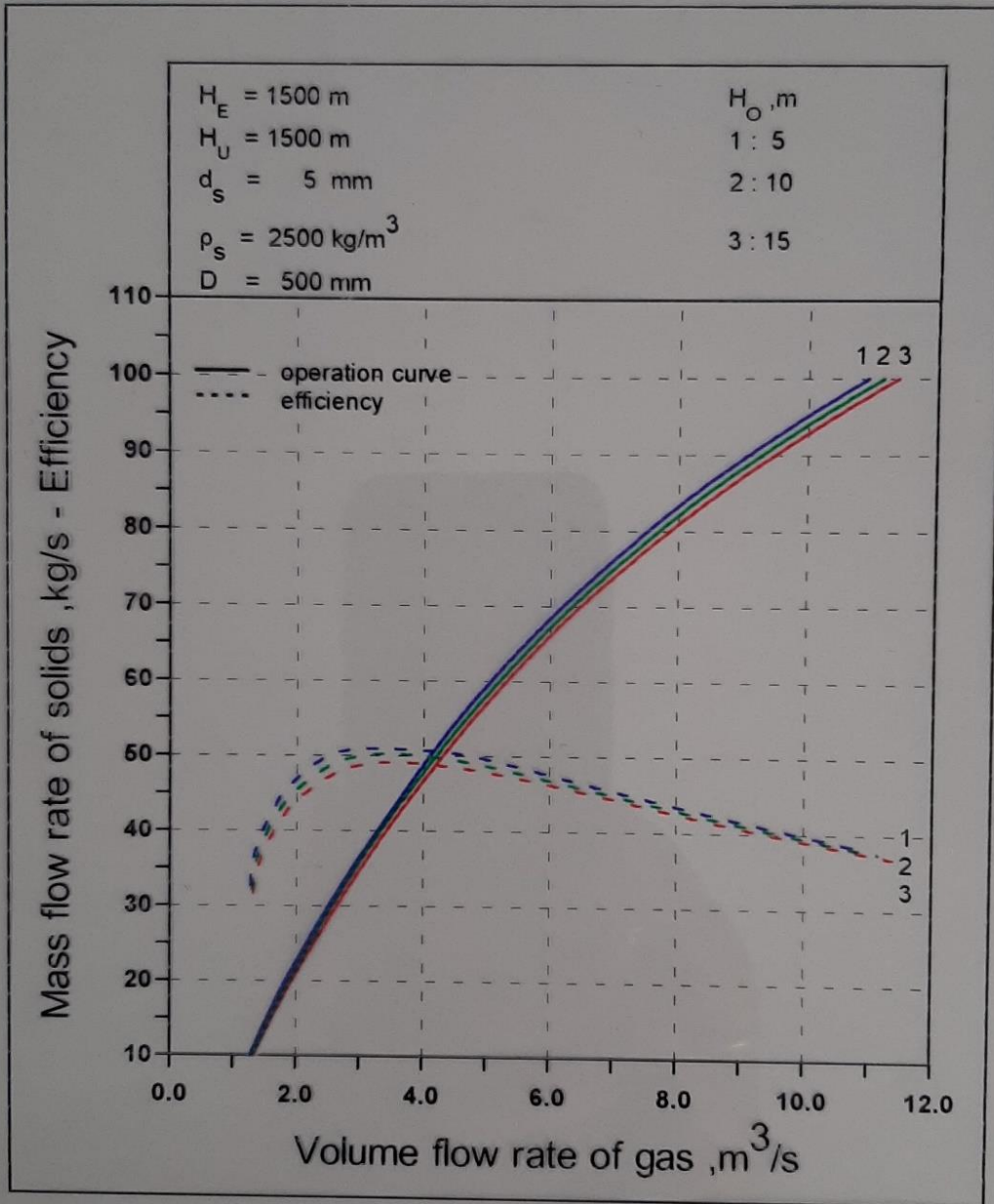
Influence of injection depth  
on Air - Lift pump operation



Influence of particle density on Air - Lift pump operation



Influence of particle diameter  
on Air - Lift pump operation



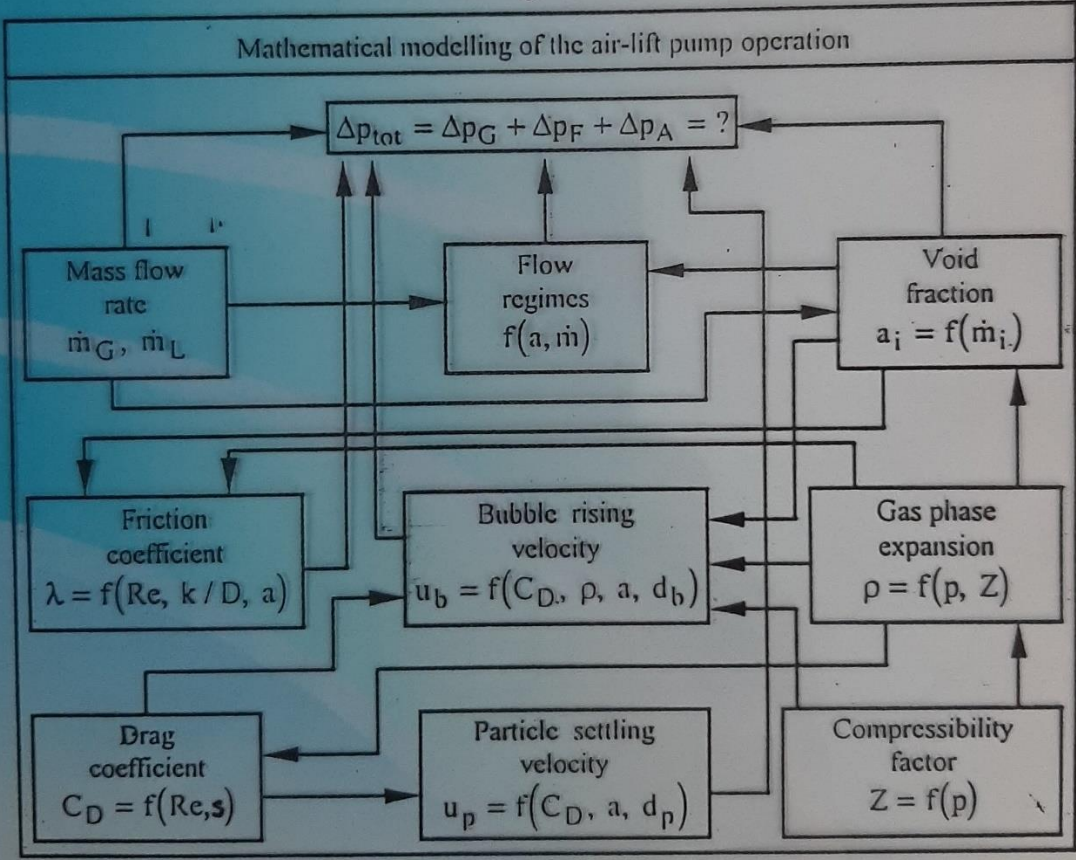
Influence of discharge height  
on Air - Lift pump operation



# DESIGN OF AN AIR-LIFT PUMP

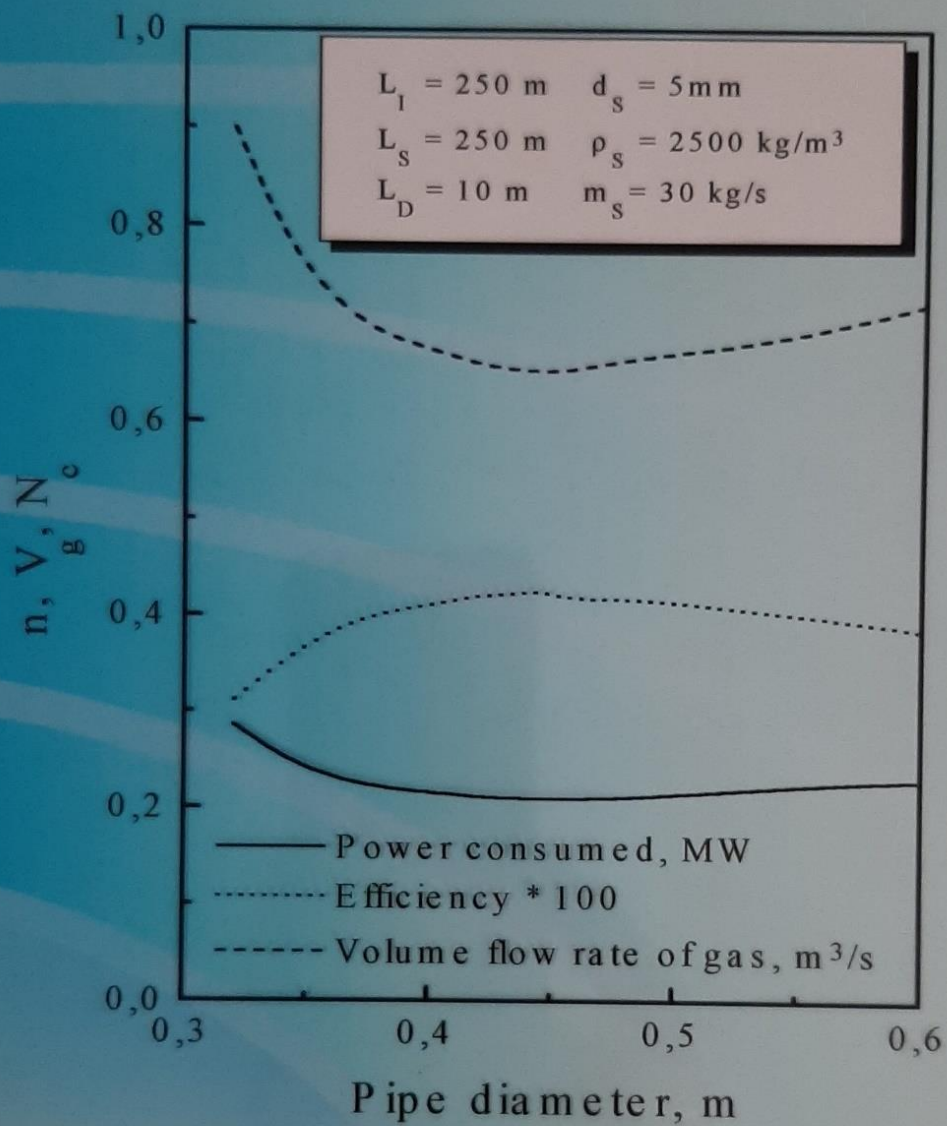
Mass flow rate of solids,  $\dot{m}_s$   
 Particle properties,  $\rho_s, d_p$   
 Height of rising,  $H_{tot}$

INPUT



OUTPUT

$\dot{m}_s = f(Q_G)$   
 $P_{min} = f(D, H_I)$



Βελτιστοποίηση λειτουργίας υδροπνευματικής αντλίας